

## BACKGROUND

- Self-associating (SA) molecules have both electron pair donor and acceptor sites, and can form hydrogen bonds with themselves
- Molecules with only donor- or only acceptor sites, such as ethers, ketones, and esters, are nonself-associating (NSA), but can form hydrogen bonds with other molecules → **cross-association**
- Traditional SAFT parameterisation only treats SA molecules explicitly
- Need approach to obtain association parameters for NSA molecules

## OBJECTIVE

To develop a general and physically consistent approach to account for cross-association in a predictive manner for a wide range of components

## METHODOLOGY

### STEP 1: Select thermodynamic model

- SAFT-VR Mie-GV [1] combines SAFT-VR Mie [2] with the dipolar term of Gross & Vrabec [3]
- SAFT-VR Mie-GV accurately describes properties of dipolar molecules, therefore serves as suitable foundation of this work
- A single electron pair donor site (N scheme) is assigned to the polar, NSA molecules that will allow them to cross-associate [4,5]

### STEP 2: Select tool to determine association parameters

- Discretised sensitivity analysis [4,5] is used to determine suitable association parameters
- The SAFT-VR Mie-GV parameters are fixed, and the association parameters ( $\epsilon^{AB}$  and  $r_c$ ) are varied at discrete intervals
- Mixture VLE is calculated at each combination of ( $\epsilon^{AB}$ ,  $r_c$ )
- The deviations are projected onto the ( $\epsilon^{AB}$ ,  $r_c$ )-plane, resulting in contour plots (see Fig. 1(a))
- In this work an “alcohol-first” approach is followed: binary VLE of alcohol + ether/ketone/ester systems are used in the development

### STEP 3: Analysing discretisation results

- ( $\epsilon^{AB}$ ,  $r_c$ )-pairs on the same contour give almost identical predictions
- Ketone/ether mixtures: minimum AAD locus (white line in Fig. 1(a)) is similarly located for all investigated systems → can use **global** parameter set for homologous group
- For ester mixtures,  $\epsilon^{AB} = f(r_c^{\text{alcohol}}, M_w^{\text{ester}})$

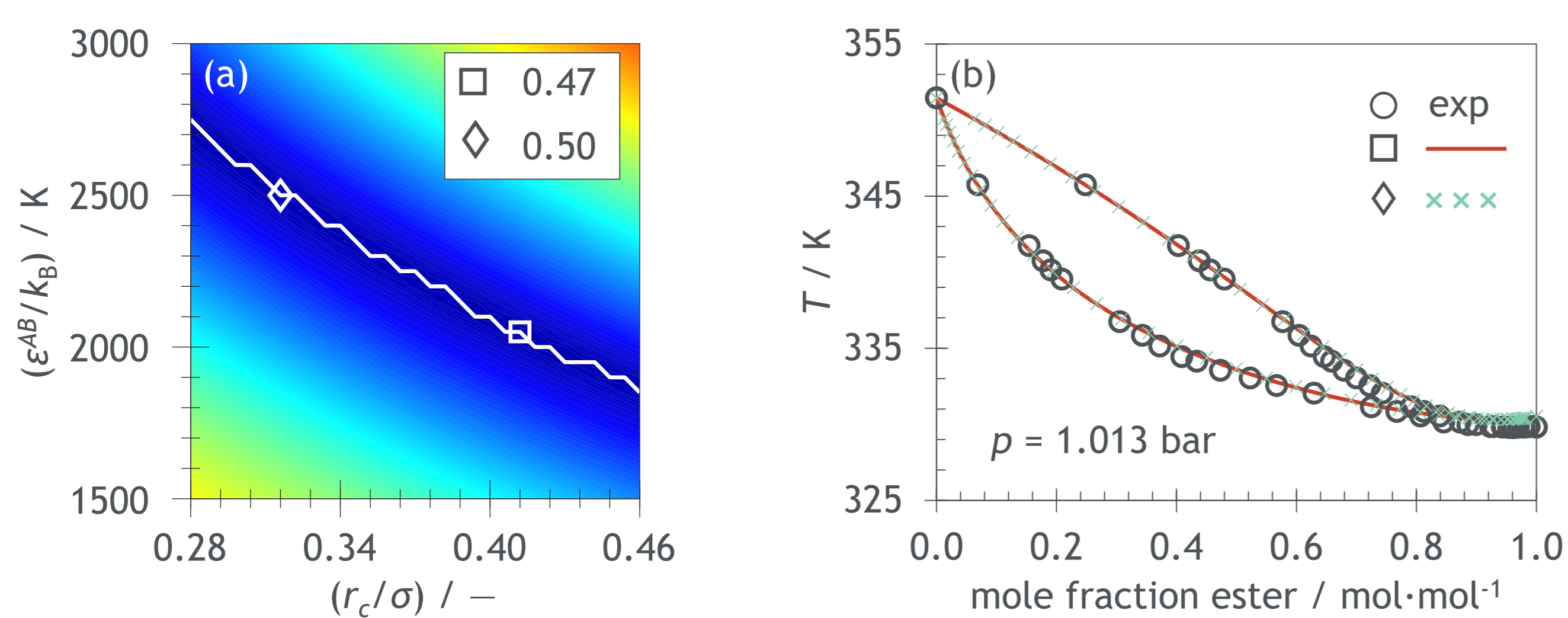


Fig. 1. Contour plot (a) and corresponding predictions (b) for methyl ethanoate + ethanol. Data from Ref. [6].

## RESULTS

### 1. Extended temperature/pressure ranges

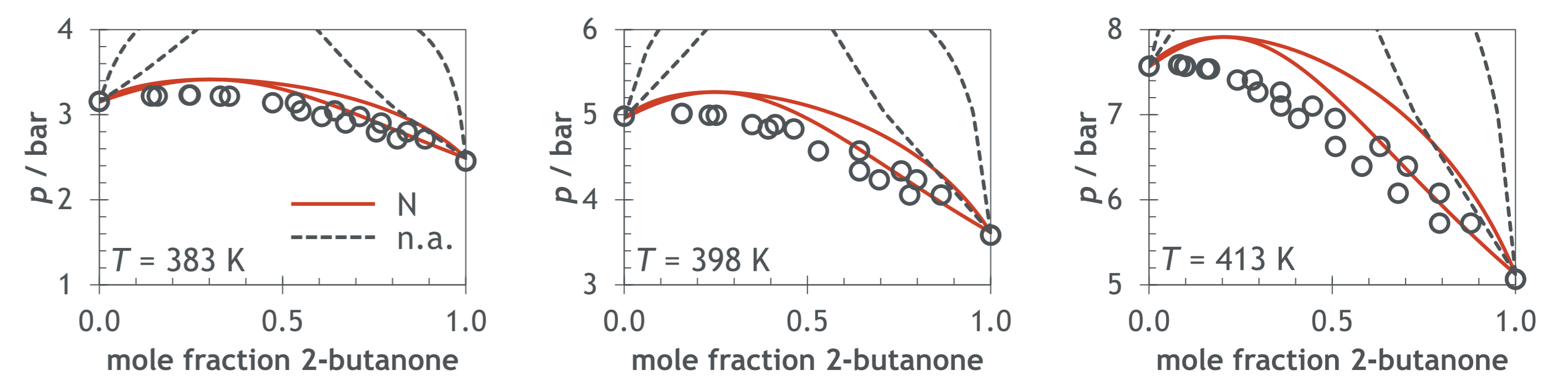


Fig. 2. 2-Butanone + ethanol VLE at three temperatures. Data from Ref. [7].

- Results indicate temperature dependence of association parameters
- Highlights potential shortcoming of association term

### 2. Molecules not included in method development

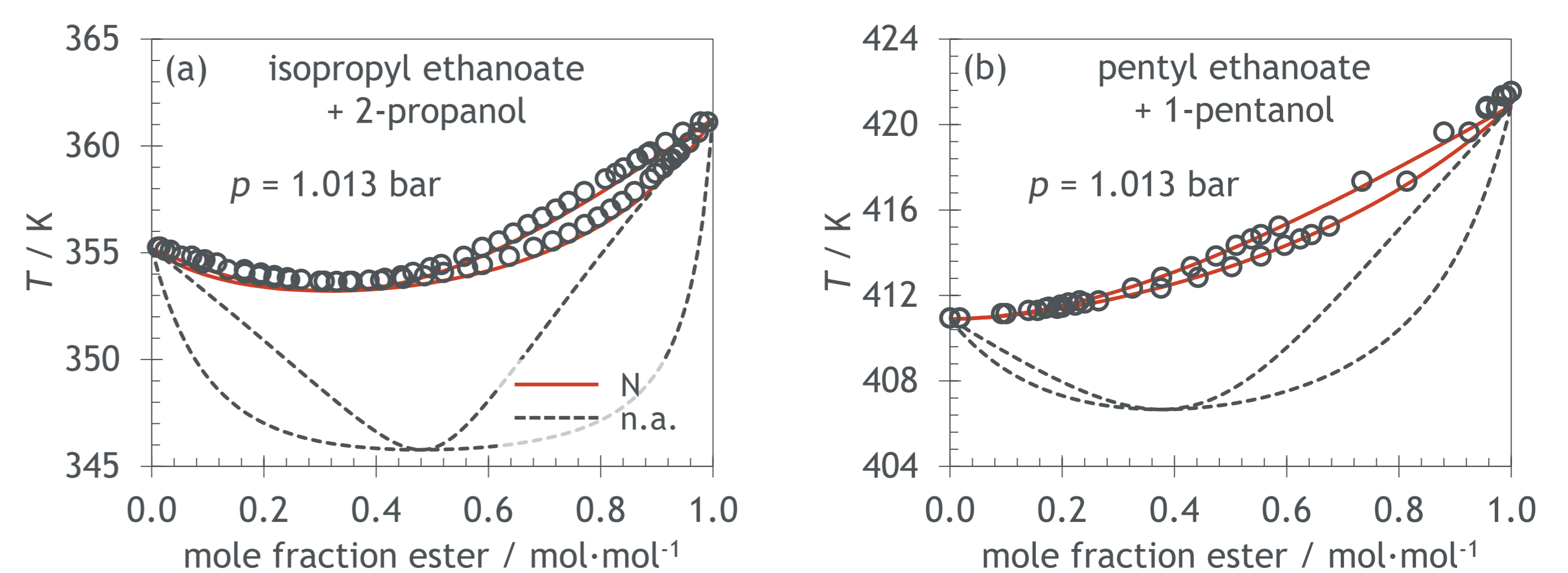


Fig. 3. (a) Isopropyl ethanoate + 2-propanol [8]; (b) Pentyl ethanoate + 1-pentanol [9].

- Application **beyond** components used in the method development support validity of approach and correlation used for esters

### 3. Aqueous mixtures

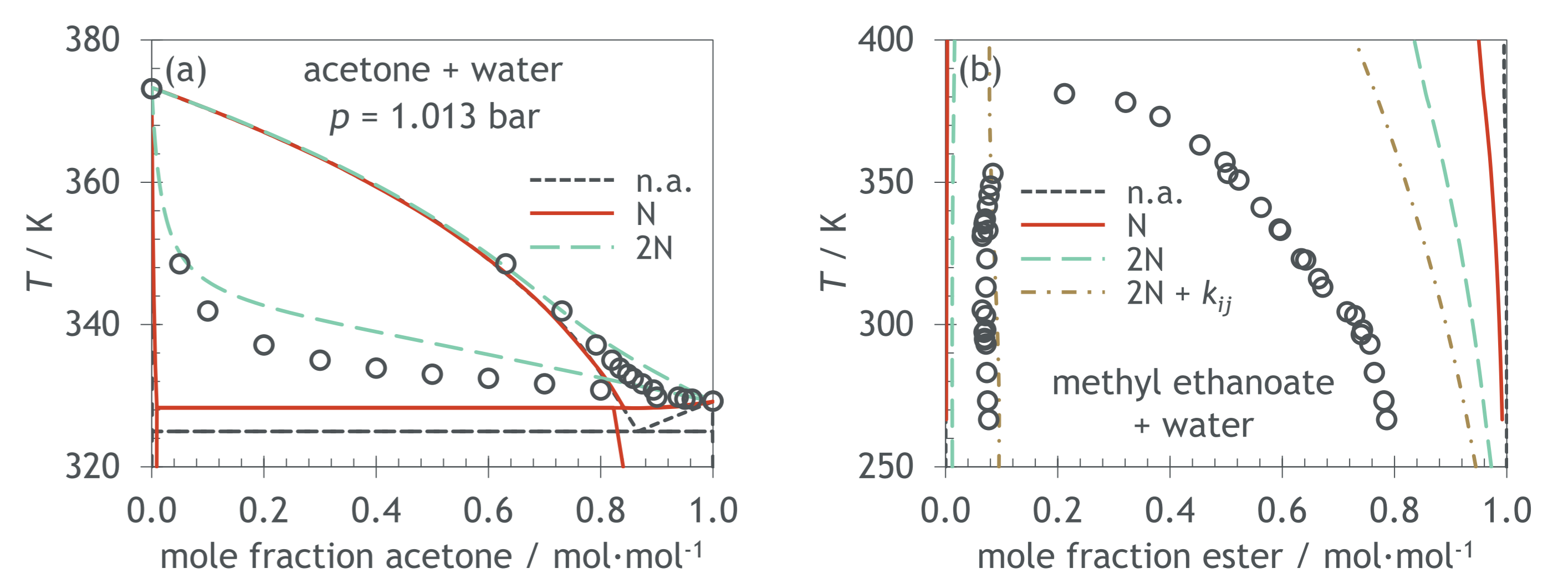


Fig. 4. (a) Acetone + water VLE [10]; (b) Methyl ethanoate + water LLE [11,12].

- Two negative sites (2N) required for qualitative VLE description
- LLE description lacking, even with inclusion of  $k_{ij}$

### 4. Mixtures with chloroform

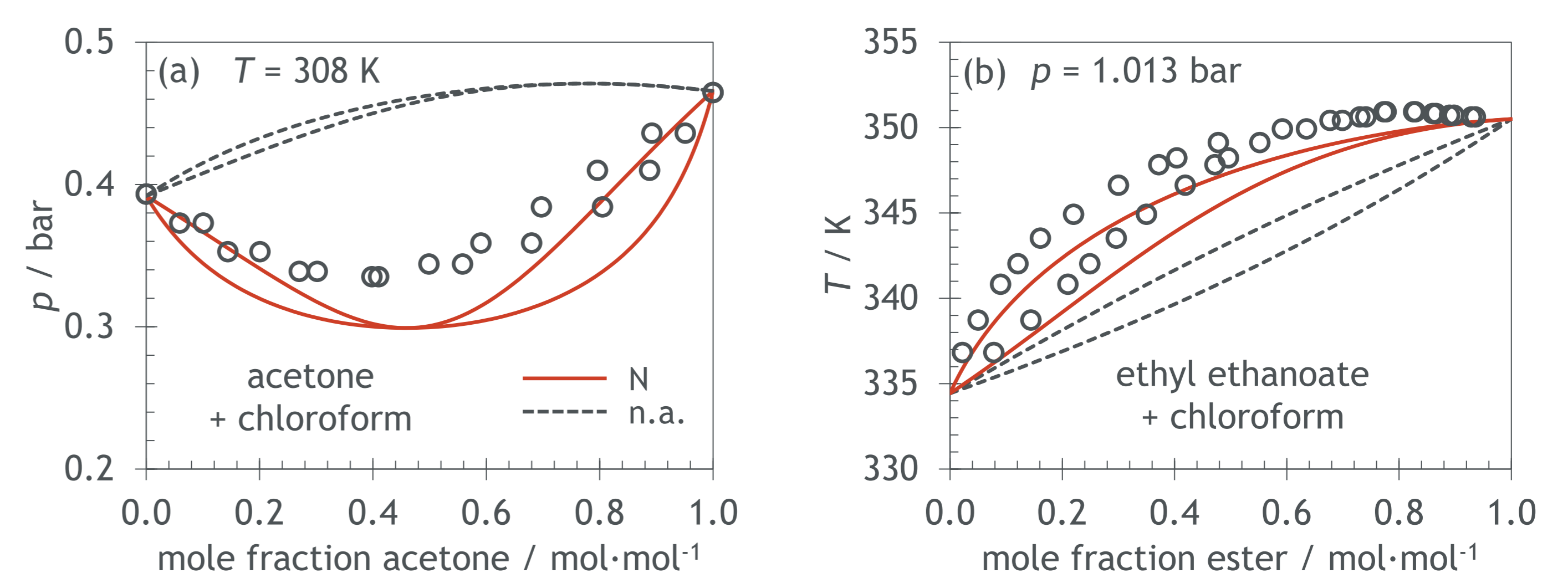


Fig. 5. (a) Acetone + chloroform [13]; (b) Ethyl ethanoate + chloroform [14].

- Obtain correct qualitative description using P-scheme for chloroform

## CONCLUSIONS

- Cross-association offers predictive approach for solvating systems
- Approach can extrapolate to components not involved in development
- Temperature dependence of association contribution evident
- Description of aqueous mixtures remains difficult

**References:** [1] *Fluid Phase Equilib.* 455 (2018): 24-42; [2] *J. Chem. Phys.* 139 (2013): 154504; [3] *AIChE J.* 52 (2006): 1194-1204; [4] *Fluid Phase Equilib.* 483 (2019): 1-13; [5] *Fluid Phase Equilib.* 569 (2023): 113775; [6] *J. Chem. Eng. Data* 35 (1990): 350-352; [7] *J. Chem. Eng. Data* 58 (2013): 1280-1287; [8] *Fluid Phase Equilib.* 287 (2010): 84-94; [9] *J. Chem. Eng. Data* 55 (2010): 2349-2354; [10] *J. Chem. Eng. Jpn.* 4 (1971): 311-318; [11] *International Critical Tables* 3 (1928): 387; [12] *Pol. J. Chem.* 54 (1980): 1101-1104; [13] *Fluid Phase Equilib.* 56 (1990): 285-301; [14] *J. Chem. Eng. Data* 7 (1962): 367-373.

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